Amendments to the Specification:

Please add the following <u>new</u> paragraph at page 1, after the title of the application:

This application is the U.S. national phase application of PCT International Application No. PCT/GB2003/004622, filed October 23, 2003, and claims priority of British Patent Application No. 0225961.2, filed November 7, 2002.

Please add the following heading at page 1, line 1:

FIELD OF THE INVENTION

Please add the following heading at page 1, line 6:

BACKGROUND OF THE INVENTION

Please add the following heading at page 3, line 9:

SUMMARY OF THE INVENTION

Please add the following headings and <u>new</u> paragraphs at page 4, before line 1:

BRIEF DESCRIPTION OF THE DRAWINGS

The invention is illustrated by reference to the accompanying drawings in which;

Figure 1 is a schematic of one embodiment of the invention whereby Fischer-Tropsch tail gas and hydrocarbon feedstock are added separately to the primary reformed gas to form the secondary reformer feed stream,

Figure 2 is a schematic of a second embodiment of the invention where, in addition to Fischer-Tropsch tail gas and hydrocarbon, carbon dioxide separated from secondary reformed gas is added to the primary reformed gas to form the secondary reformer feed stream,

Figure 3 is a schematic of a third embodiment of the invention whereby Fischer-Tropsch tail gas and hydrocarbon feedstock are combined, heated and added to the primary reformed gas to form the secondary reformer feed stream.

Figure 4 is a table that contains data calculated for a Fischer-Tropsch process operated in accordance with the schematic depicted in Figure 2.

Figure 5 is a table that contains data calculated for a 80,000 barrel-per-day Fischer Tropsch process operated in accordance with the schematic depicted in Figure 3.

DETAILED DESCRIPTION OF THE INVENTION

Please delete the paragraphs at page 9, line 33 through page 10, line 5.

Please replace the paragraph beginning at page 10, line 7, with the following rewritten paragraph:

In Referring now to the drawing, in Figure 1, hydrocarbon feedstock, for example natural gas | containing over 90% v/v methane, fed via line 10 is divided into two streams. The first stream is fed via line 12 to a saturator 14 where it is contacted with hot water provided by line 16. Waste hot water is recovered via line 18 and may be recycled if desired. The resulting mixture of first hydrocarbon stream and steam is fed, typically at a pressure in the range 10 to 60 bar abs., via line 20 to a heat exchanger 22 and thence, via line 24, to the catalyst-containing tubes 26 of a heat exchange reformer 28. The mixture is typically heated to a temperature in the range 300 to 500°C prior to entry into the tubes 26. For simplicity only one tube is shown in the drawing: in practice there may be several tens or hundreds of such tubes.

Please replace the paragraph beginning at page 12, line 12, with the following rewritten paragraph:

Table 1 Figure 4 is a table that contains data calculated for a Fischer-Tropsch process operated | in accordance with the flowsheet schematic depicted in Figure 2. The data demonstrates that | the process of the present invention is able to provide a steam ratio in the heat-exchange reactor tubes of 1.25 and thereby, with a nickel steam reforming catalyst avoid carbon deposition, yet based on total hydrocarbon feed to the process, the overall steam ratio is 1.0.

Please replace the paragraph beginning at page 20, line 19, with the following rewritten paragraph:

~~Table 2~~ Figure 5 is a table contains data calculated for a 80,000 barrel-per-day Fischer-Tropsch process operated in accordance with the ~~flowsheet~~ schematic depicted in Figure 3. The data demonstrated that the process of the present invention is able to provide a steam ratio in the heat-exchange reactor tubes of 0.88 and thereby, with a precious metal reforming catalyst avoid carbon deposition, yet based on total hydrocarbon fed to the process, the overall steam ratio is 0.66.

Please delete the entire Table 1 at page 13.

Please delete the entire Table 2 at page 14.